

# Optimising energy and carbon management for an AAD plant using MILP

**Harry Laing** 

Advances in the Digitalisation of the Process Industries 2021 21<sup>st</sup> October 2021

C500, Merz Court, Newcastle University
 h.j.laing@ncl.ac.uk
 @H\_Laing1

From Newcastle. For the world.

#### **Talk Outline**



- What happens to our waste? (Background)
- The Poop Processing Plant (Site Overview)
- Another Tax?! (Carbon Emissions)
- What's the point (of the app)? (Purpose)
- How does it work? (**Optimisation and Modelling Techniques**)
- The App! (Demonstration)
- Final Comments







## What happens to our waste?









#### How much?!





From Newcastle. For the world.

process intensification group

NORTHUMBRIAN WATER*living* water



## **The Poop Processing Plant**



#### **Overview of the Howdon Plant**







 $E_{GEN,1}$ 

 $E_{GEN.2}$ 

 $E_{GEN,4}$ 

#### **Biomethane Processing Plant**

- **Biomethane (Biogas)** produced form Anaerobic Digesters
- Biogas **OR** Natural Gas (not both) can be used in CHP or Boiler [CHP4 Nat Gas Only]
- **Biogas** can be enriched for Gas Injection
- Flare Stack available as last resort ٠

process intensification group



## Another Tax?!?

ncl.ac.uk

#### **Carbon Neutrality Pledge and Tax**



•	Northumbrian V	Vater Ltd pledges	to be Carbon	Neutral by 2027
---	----------------	-------------------	--------------	-----------------

- To aid/incentivise the move, NWL will incur a 'Carbon Tax' (subject to a Carbon Emissions Performance Criteria)
- Cost: £187 per tonne CO2e

Variable	Factor	Units	
Import Electricity	0 <b>or</b> 0.31	kgCO <sub>2</sub> e/kWh	
Export Electricity	-0.28307	kgCO <sub>2</sub> e/kWh	
Import Natural Gas	0.18396	kgCO <sub>2</sub> e/kg	
Export Biomethane	-2.04652	kgCO <sub>2</sub> e/m <sup>3</sup>	
Propane	1.51906	kgCO <sub>2</sub> e/L	
Diesel	2.9705	kgCO <sub>2</sub> e/m <sup>3</sup>	
Biogas CHP	0.0175	kgCO <sub>2</sub> e/m <sup>3</sup>	
Biogas residual	0.16	kgCO <sub>2</sub> e/m <sup>3</sup>	

#### **IMPROVING THE ENVIRONMENT**

Our ambitious goals in this area are to:

- Be leading in the sustainable use of natural resources, through achieving zero avoidable waste by 2025 and being carbon neutral by 2027
- Demonstrate leadership in catchment management to enhance natural capital and deliver net gain for biodiversity
- · Have the best rivers and beaches in the country
- · Have zero pollutions as a result of our assets and operations

From Newcastle. For the world.





## What's the point (of the App)?



#### **Purpose of the App**

- Operators have no way of validating their current operational strategy
- Daily Biogas production levels change based on sludge processing demands
- Electricity prices change daily ("fixed variable")
- Natural Gas prices can change seasonally

• <u>Aim</u>: To provide operators/managers with a quick tool to validate operational decisions, based on up to date pricing, biogas production and carbon emissions





#### **E.g. Varying Electrical Costs**



• Electrical Import and Export costs vary every half hour, but are fixed one day ahead for 24 hours



From Newcastle. For the world.

process intensification group





## How does it work?

ncl.ac.uk

#### How can we define the plant model?

- All flow rates and process limits can be defined as a series of linear equations
- For example: CHP Engine gas flows
  - Gas flow to a CHP engine can be either Biogas  $(B_{CHP,i,t})$  or Natural Gas  $(N_{CHP,i,t})$
  - Each unit has a maximum capable gas flow
  - Minimum gas flow is half the maximum for operation

 $B_{CHP,min} \leq B_{CHP,i,t} \leq B_{CHP,max}$ 

 $N_{CHP,min} \leq N_{CHP,i,t} \leq N_{CHP,max}$ 





Newcastle

Universitv

#### **Linear Programming Model - CHP Example**



- Gas flow must be either Biogas **OR** Natural Gas
- Use a binary variable,  $z_{i,t}$  (= 1 or 0), to force this choice

$$B_{CHP,min} \cdot \mathbf{z}_{i,t} \leq B_{CHP,i,t} \leq B_{CHP,max} \cdot \mathbf{z}_{i,t}$$

$$N_{CHP,min} \cdot (1 - \mathbf{z}_{i,t}) \leq N_{CHP,i,t} \leq N_{CHP,max} \cdot (1 - \mathbf{z}_{i,t}) \qquad \mathbf{z}_{i,t} = \mathbf{0}$$

 $z_{i,t} = 1$ 



## **Linear Programming Model - CHP Example**



- In addition, the engines can either be **On** or **Off**
- Use two more binary variables,  $w_{i,t,1}$  and  $w_{i,t,2}$ , to force this choice

 $B_{CHP,min} \cdot z_{i,t} - B_{CHP,min} \cdot w_{i,t,1} \leq B_{CHP,i,t} \leq B_{CHP,max} \cdot z_{i,t} - B_{CHP,max} \cdot w_{i,t,1}$ 

 $N_{CHP,min} \cdot (1 - z_{i,t}) - N_{CHP,min} \cdot \boldsymbol{w}_{i,t,2} \leq N_{CHP,i,t} \leq N_{CHP,max} \cdot (1 - z_{i,t}) - N_{CHP,max} \cdot \boldsymbol{w}_{i,t,2}$ 



#### From Newcastle. For the world.

process intensification group

## **Linear Programming Model - CHP Example**

- Further, must now consider engine start-up, shutdown and minimum operating time once switched on
- Use four more binary variables,  $su_{i,t,1}$ ,  $su_{i,t,2}$ ,  $sd_{i,t,1}$  and  $sd_{i,t,2}$

 $B_{CHP,min} z_{i,t} - B_{CHP,min} w_{i,t,1} - 0.5B_{CHP,min} su_{i,t,1} - 0.5B_{CHP,min} sd_{i,t,1} \le B_{CHP,i,t}$ 

 $B_{CHP,i,t} \le B_{CHP,max} \ z_{i,t} - B_{CHP,max} \ w_{i,t,1} - 0.5B_{CHP,max} \ su_{i,t,1} - 0.5B_{CHP,max} \ sd_{i,t,1}$ 

 $N_{CHP,min}(1 - z_{i,t}) - N_{CHP,min} w_{i,t,2} - 0.5 N_{CHP,min} su_{i,t,2} - 0.5 N_{CHP,min} sd_{i,t,2} \le N_{CHP,i,t}$ 

 $N_{CHP,i,t} \le N_{CHP,max}(1-z_{i,t}) - N_{CHP,max} w_{i,t,2} - 0.5N_{CHP,max} su_{i,t,2} - 0.5B_{CHP,max} sd_{i,t,2}$ 







## **Mixed Integer Linear Programming (MILP)**



 MILP takes a series of linear statements (equalities and inequalities) and aims to minimise a cost function.

$$\min_{x} f^{T}(x) \text{ subject to} \begin{cases} x(intcon) \\ A \cdot x \leq b \\ Aeq \cdot x = beq \\ lb \leq x \leq ub \end{cases}$$

• <u>Aim</u>: to minimise expenditure (maximise potential profits) of our plant based on energy, gas and carbon use/distribution



#### **Mixed Integer Linear Programming (MILP)**



• For a single 24 hour optimisation (48 half hourly time periods):





## The App!

ncl.ac.uk

#### The App! General Use



From Newcastle. For the world.

process intensification group





Key Variables:

- 38,000 Nm<sup>3</sup> Biogas / Day
- Nat Gas 65 p/therm

	Current Operation	Optimal Operation
Total Revenue	£ 8350	£ 9270
Revenue Excluding Carbon	£ 12390	£ 7927
Cost of Carbon	£ 4040	<b>£</b> -1343
		Ŷ

Carbon Tax Payable in two years time



#### **Comparison to Current operation**



	<b>Current Operation</b>	Optimal Operation
Total Revenue	£ 8350	£ 9270
Revenue Excluding Carbon	£ 12390	£ 7927
Cost of Carbon	£ 4040	<b>£</b> -1343





From Newcastle. For the world.

process intensification group





Key Variables:

- 38,000 Nm<sup>3</sup> Biogas / Day
- Nat Gas 65 p/therm

	Current Operation	Optimal Operation	Current Annual	Optimal Annual
Total Revenue	£ 8350	£ 9270	£ 3.05 M	£ 3.38 M
Revenue Excluding Carbon	£ 12390	£ 7927	£ 4.52 M	£ 2.89 M
Cost of Carbon	£ 4040	£ -1343	£ 1.47 M	£ -0.49 M
		Υ	J	

Carbon Tax Payable in two years time





## **Final Comments**

ncl.ac.uk



- Provides quick optimisations
- Validates operational decisions
- Allows operators/managers to investigate scenarios easily
- Highlights the importance of new legislation (Carbon Tax)
- Demonstrates impactful changes could be made to operational strategy, especially with respect to daily revenues





- Retrospective Analysis
  - Investigate unprecedented energy prices

- Investigation into CHPQA and it's impact on annual operations
  - CHPQA can be considered a tax relief based on the usage on CHP Engines

- With some adaptations, model could be **applied to similar sites** (Such as the Bran Sands site at NWG)
  - Funding secured to implement and deploy models within NWL





# NORTHUMBRIAN WATER (iving water



Shaping careers, delivering innovation







## Thank you for listening Any Questions?

Ħ

田

C500, Merz Court
h.j.laing@ncl.ac.uk
@H\_Laing1



process intensification group

ncl.ac.uk