

Lessons Learned Database

Individual Incident Summary Report



Incident Title		FCC Explosion and Asphalt Fire	
Incident Type		Explosion and Fire	
Date		26 th April 2018	
Country		USA	
Location		Superior, WI	
Fatalities		Injuries 36	Cost US\$ 457 m (2021) – Ref. 2
Incident Description	The pr		orber towers at the Fluid Catalytic
	Cracking (FCC) unit exploded while it was being shut down for a planne maintenance turnaround. More than 100 metal fragments were propelled u to 366 m (1200 ft) away. Explosion debris punctured the top section of		
	nearby asphalt tank. Over the next 2 hours, approx. 2780 m ³ (17,000 barrels) leaked out of the hole and spread through the refinery. The asphalt ignited and multiple large fires erupted in several operating areas of the refinery.		
	The City of Superior (WI), in which the refinery is located, evacuated 2507 residents because of the potential for release of highly toxic hydrofluoric (HF)		
Credit: WDIO ABC News/US CSB	acid. The nearby City of Duluth (MI) issued a shelter in place advisory.		
	Fortunately, the HF storage vessel was not damaged even though it was		
Incident Analysis	located closer to the epicentre of the explosion(s) than the asphalt tank. Basic cause of the 2 explosions was brittle fracture of the primary absorber		
Incluent Analysis	and sponge absorber due to inadvertent mixing of air and hydrocarbon and ignition by pyrophoric material in the vessels. Basic cause of the large asphalt fire was believed to be pyrophoric material inside the asphalt tank smouldering on exposure to air entering through the punctured tank wall.		
	Critical factors included: 1) The FCC was in transient operation mode, 2) The regenerator pressure was higher than the reactor and main fractionator		
	pressures during the transient, 3) The spent catalyst slide valve (SCSV) internals were severely eroded (increased leak rate), 4) A "steam barrier" had not been established in the reactor to keep air (in regenerator) separated		
	from hydrocarbons (in main fractionator), 5) A main fractionator "gas purge" to remove oxygen from the system had been omitted, 6) One (reciprocating)		
	wet gas compressor was still running, 7) The absorbers were constructed		
	from a grade of steel susceptible to brittle fracture, 8) The asphalt tank bund		
	was too close to the tank (head pressure created leak path above the bund).		
	Root causes included: 1) Inadequate hazard identification (air leakage from		
	regenerator to reactor to main fractionator), 2) Inadequate transient operation safeguards (catalyst slide valves, steam barrier, gas purge), 3) Inadequate		
	instrumentation (differential pressures between inter-connected vessels), 4) Inadequate shutdown procedures (incorrect pressure profile specified across		
	unit), 5) Inadequate operator training (hazard awareness, abnormal situation response, venting, purging), 6) Inadequate process safety management		
	(reliance on in-house FCC knowledge, limited use of external expertise).		
Lessons Learned	 Transient operations (e.g. startup, shutdown, safe park) on process plant may require different safe operating limits compared with normal operation. Process hazard analysis (PHA) studies (e.g. Hazop) should consider hazards arising during transient conditions as well as normal operation. FCC reactor pressure should exceed regenerator and main fractionator in transient mode until an isolation blind is inserted at the fractionator inlet. Materials exhibiting ductile behaviour in all operating modes are inherently safer than those exhibiting brittle behaviour in extreme (transient) conditions. 		
More Information	1) "FCC Unit Explosion and Asphalt Fire at Husky Superior Refinery", US		
	Chemical Safety and Hazard Investigation Board, Report No. 2018-02-I-WI		
	 (2022): <u>https://www.csb.gov/husky-energy-superior-refinery-explosion-and-fire/</u>. 2) "100 Largest Losses in the Hydrocarbon Industry", Marsh Property Risk 		
	Consulting Practice, 27th Edition (2022).		
Industry Sector		Process Type	Incident Type
Oil & Gas		Fluid Catalytic Cracking	Explosion & Fire
Equipment Category		Equipment Class	Equipment Type
Mechanical		Vessel	Absorber