

Lessons Learned Database

Individual Incident Summary Report



Incident Title		Absorber/Stripper Reflux Cooler Bypass Rupture	
Incident Type		Fire and Explosion	
Date		9 th November 1992	
Country		France	
Location		La Mède	
Fatalities		Injuries	Cost
6		38 (1 serious)	US\$ 575 m (2021) – Ref. 2
Incident Description	On 09-	Nov-92 with the Fluid Catalytic Cra	cker Unit (FCCU) running normally,
	a DN 2	200 (8" NS) bypass line around th	ne Unsaturated Gas Plant (USGP)
	absorb	er/stripper reflux cooler suddenly	ruptured. Approximately 12 tonnes
	(26,50	0 lbs) of light hydrocarbons were	released over a 10-minute period,
	creatin	g a vapour cloud covering an area	of around 14,000 m ² (150,000 ft ²)
and the second sec	and er	igulfing several process units. The	e cloud reached a fired heater and
	explod	ed. The resulting overpressure call	Ised massive damage to the FCCU
		SGP and the root of the local con	lior room conapsed, killing 5 of its
Credit: Ministry of Environment/BARPI	The refinery fire brigade and over 100 external firefighters from neighbouring		
	industrial sites and towns took 6 hours to extinguish or bring most of the fires		
	under control but some were left burning to allow safe depressurisation of		
	the process units because the flare system had suffered explosion damage.		
	The whole refinery was shut down for several months and the FCC and the		
	USGP took a year to rebuild. A nearby town also suffered property damage.		
Incident Analysis	Basic cause was rupture of the carbon steel absorber/stripper reflux cooler		
	bypass line due to uniform internal corrosion which led to a loss of primary		
	containment (LOPC) and a vapour cloud explosion (VCE).		
	Critical factors included: 1) The local control room (built in 1953) had not		
	been designed to be blast-resistant, 2) Proximity of occupied buildings (e.g.		
	local control room) and other process equipment (e.g. tanks) to the epicentre		
	of the explosion, 3) The failed pipe was original equipment (started up in		
	1956) and had not been regularly inspected because it was a bypass line.		
	Root causes included: 1) Poor plant layout and inadequate equipment		
	spacing (occupied buildings and storage tanks too close to ECC/USCP) 2)		
	Inadequate process hazard analysis (impact of fire and blast wave exposure		
	on adjacent process plant), 3) Inadequate hazard awareness (corrosion in		
	dead-legs), 4) Inadequate inspection (corrosion monitoring), 5) Inadequate		
	process safety management (absence of engineering authority role).		
Lessons Learned	1) Occupied buildings should be sited outside areas where thermal effects		
	or overpressure could cause significant damage to the building and/or should		
	be constructed to be sufficiently blast-resistant to mitigate any material risk.		
	2) Worst case scenario studies (including escalation) should be carried out		
	to inform plant design (e.g. plant layout, equipment spacing, active/passive fire protection, etc) and emergency response planning strategies		
	3) Robust management of change (MoC) criteria should be applied to any		
	proposal to site new/modified equipment near large potential sources of leak		
	4) Process units and piping systems should be systematically reviewed and		
	field-checked to identify and (where practicable) eliminate dead-legs.		
	5) Piping in dead-legs which cannot be eliminated and piping fabricated to		
	superseded material specifications should be subject to enhanced inspection.		
More Information	1) "Gas Explosion in the Cat Cracking and Gas Plant Units of a Refinery" -		
	ARIA 3969 (2008). https://www.aria.developpement-durable.gouv.fr/wp-		
	content/files mt/FD 3969 La Mede 1992 ang.pdf.		
	2) TOU Largest Losses in the Hydrocarbon industry, Marsh Property Risk Consulting Practice, 27th Edition (2022)		
	3) "Integrity Management: Learning from Past Maior Industrial Incidents".		
F. Gil and J. Atherton, BP Process Safety Booklet #14, 2 nd Edition			/ Booklet #14, 2 nd Edition (2006).
Industry Sector		Process Type	Incident Type
Oil & Gas		Fluid Catalytic Cracking	Fire & Explosion
Equipment Category		Equipment Class	Equipment Type
Mechanical		Piping	Pipe