

**Doubling the yield of a gas-liquid
acylation process with
intensified continuous reactor
- an industrial case study**

Producing a Valuable Product takes 5 days at only 40% yields

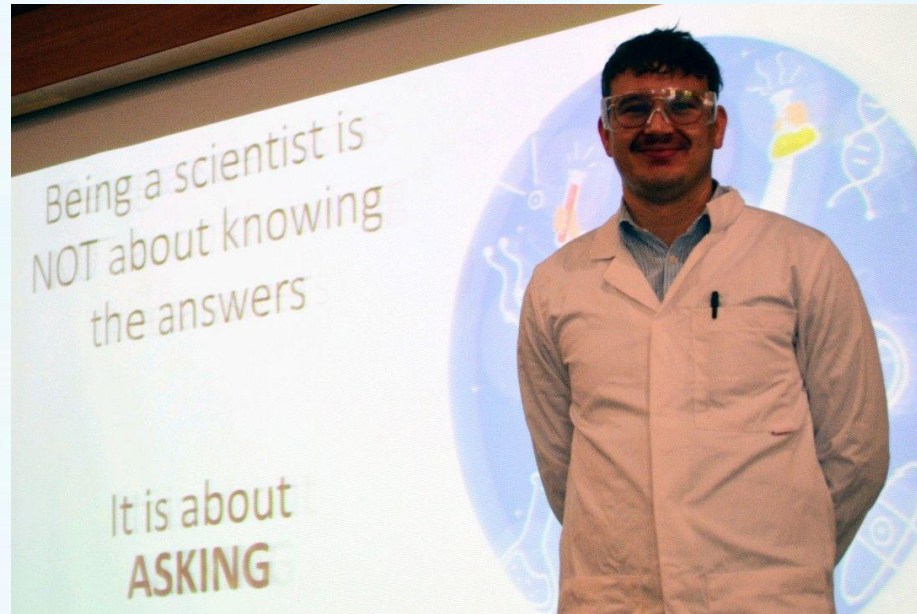
- Fragrance and flavouring product is highly valuable



- Product is sensitive to temperature but reaction is highly exothermic
- High possibility to overreact forming heavier components
- Energy intensive multi-step process

Jonty Thornton

Chemical Engineer, Stoli Chem, UK



Ask me about



- Blues Guitar
- Arsenal
- Chemical Engineering



Education and career



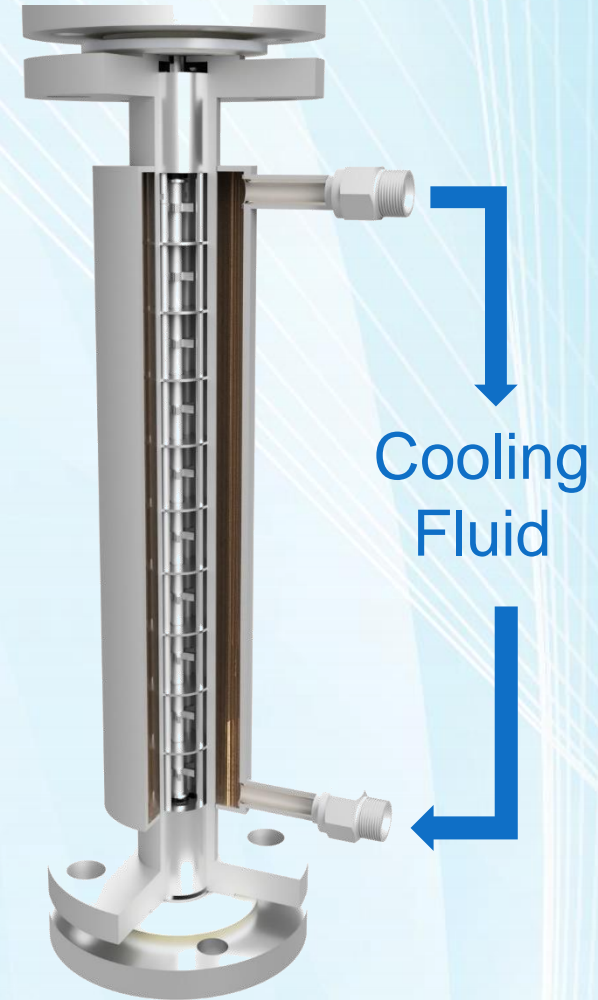
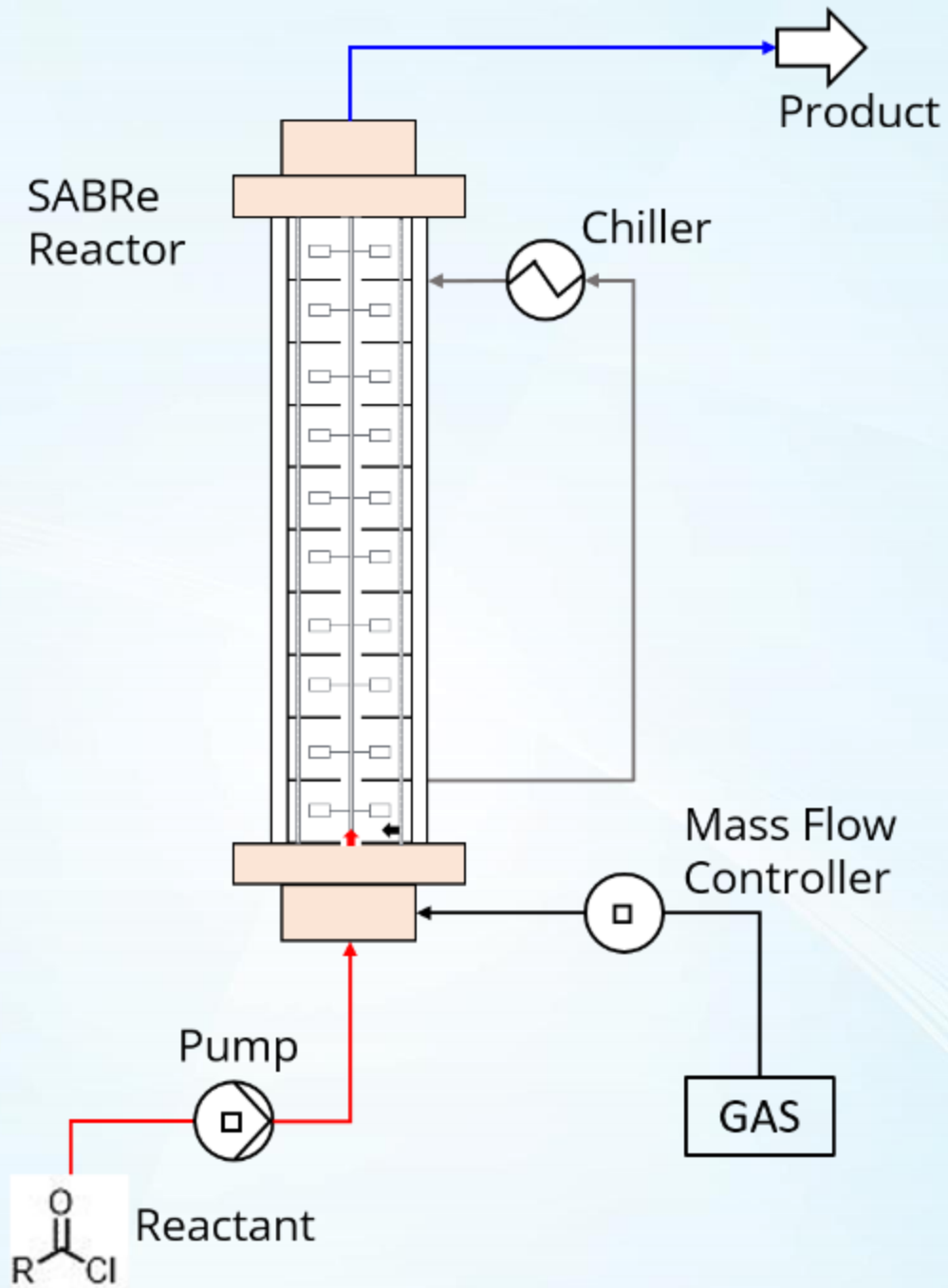
- Galaxy Kayaks – logistics operator
- University of Sheffield (2016-2021)
- Faurecia – Improvements Engineer (2019-2020)
- Quality Teach – Tutor (2021-2022)
- Stoli Chem – Chemical Engineer (2022-2024)



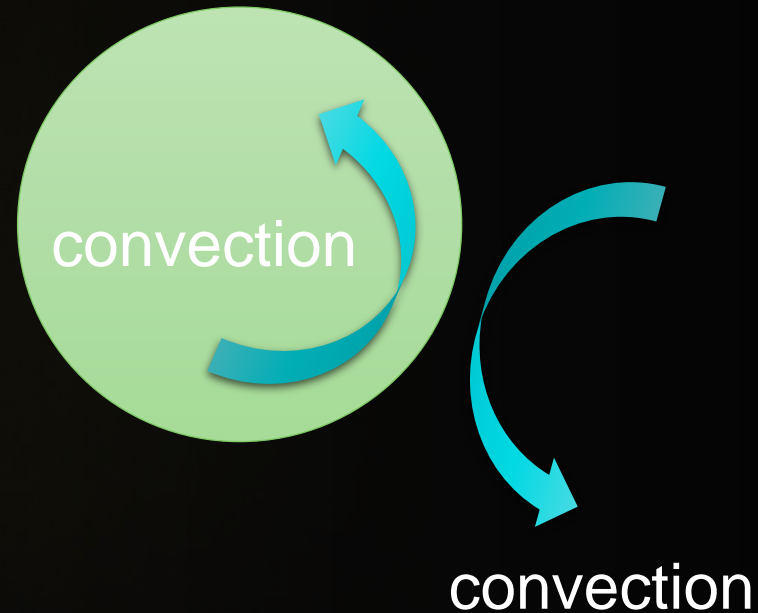
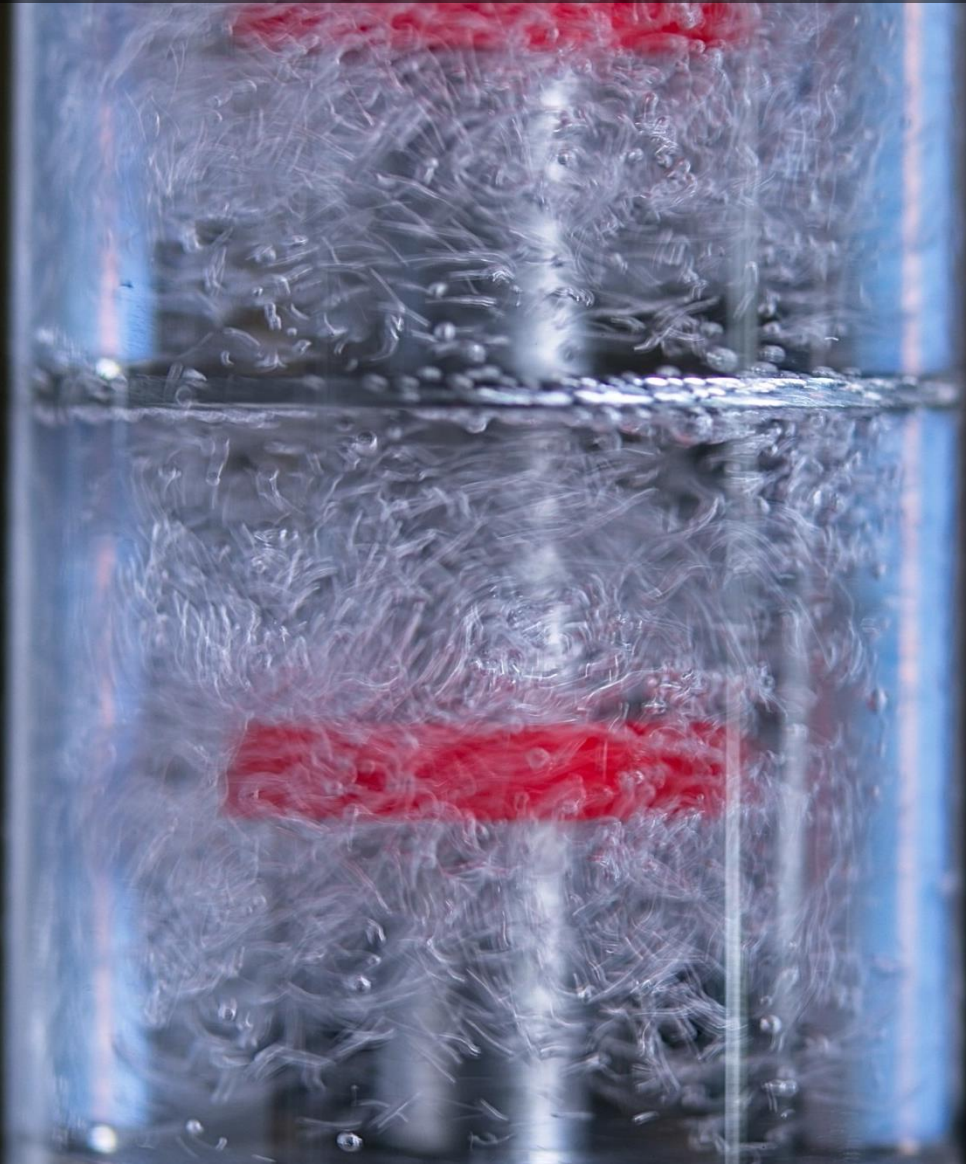
Interest

- Sports – football and cricket
- Cooking
- History
- Learning new things (science, music)

Using lab SABRe system as a potential solution



The key to interfacial mass transfer is large area and fluid movement



$$\text{rate} = k_L a \Delta C$$

~ mixing energy

Multi-dimensional Process Optimisation

- Mixing Energy
 - How does mixing intensity affect performance?
- Catalyst Amount
 - How much/little catalyst we can utilise to still be profitable, in solution and safe?
- Concentration of reactant in solvent
 - How are reaction rates and downstream purification affected by this?
- Residence time
 - How fast can the reaction get? What size reactor do we need at scale to meet customer demands?

Factors affecting gas concentration

- Gas Ratio
 - Does having a molar excess provide
- Temperature
 - How does varying temperature affect performance? Does gas solubility come into play?
- Pressure
 - What trade off can we afford between high pressure and expensive equipment?

Initial yields of only 20%

- Initial experimentation indicated low valuable product

Concentration (wt%)	Residence time (min)	Temperature (oC)	Mixing RPMs	Catalyst Molar Ratio	Molar Ratio of Propylene	Pressure (bar)
8	30	0	300	0.75	1	Ambient

Conversion (%)	Selectivity (%)	Yield (%)
80	37	20

Residence time control allows for improved reaction

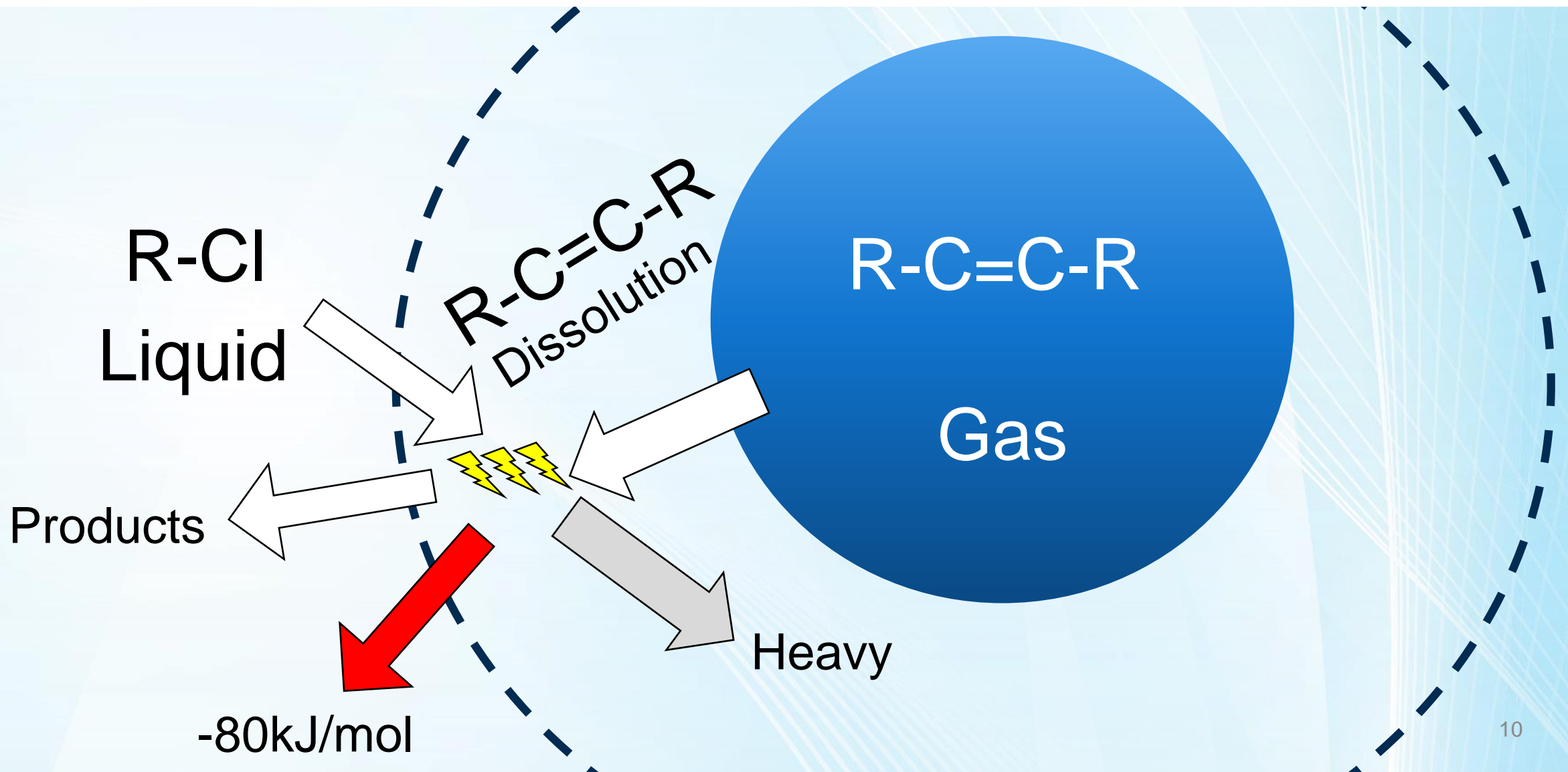


Conversion (%)	Selectivity (%)	Yield (%)
89	66	59



Mass transfer enables reaction

Heat transfer enables fast residence times



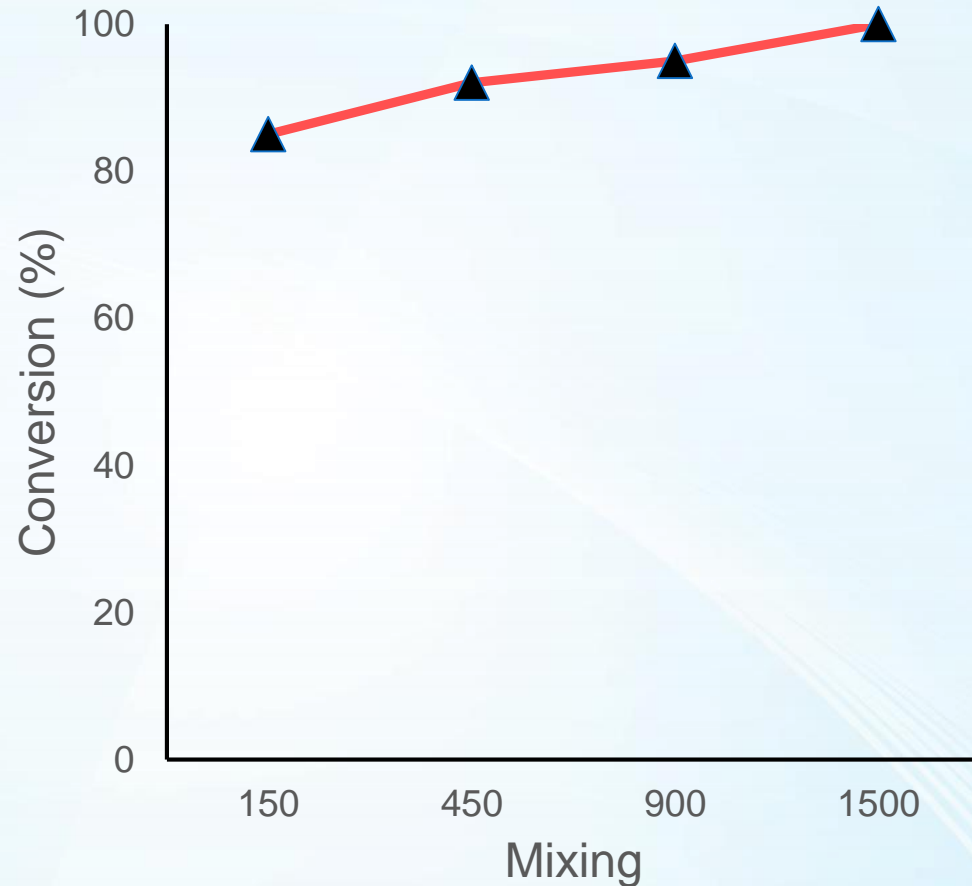
Catalyst amount – an engineering compromise

- Gambacorta and co suggests that high stoichiometry amounts typical for reaction.
- 1.2 molar ratio is our cap for catalyst – since solution is saturated
- On testing this out – just like with penicillin, Teflon and Vaseline

Conversion (%)	Selectivity (%)	Yield (%)
99.9	82	82

- More catalyst = 20% increase in yield. No brainer

Kinetically limited regime

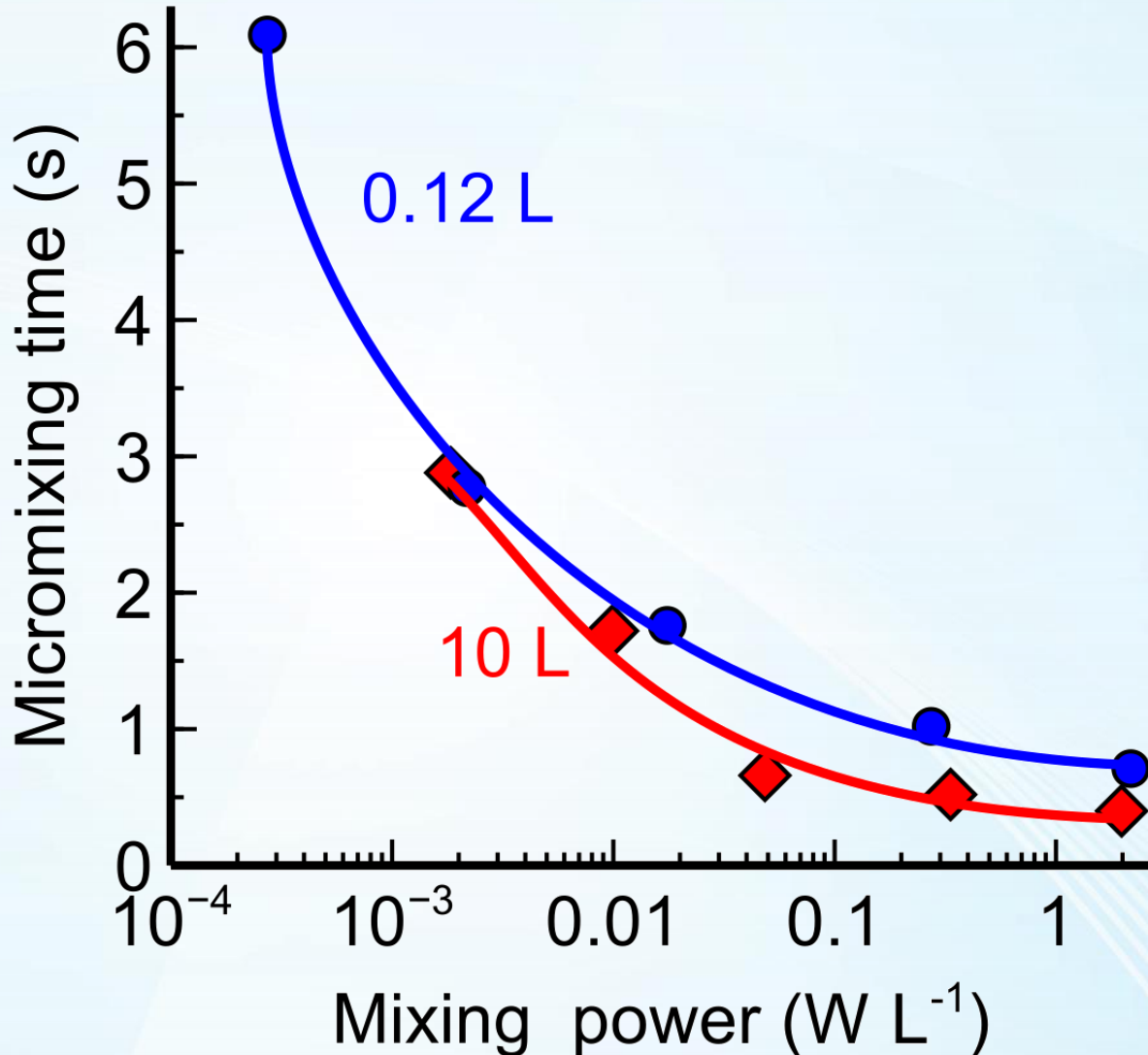


- Reducing mixing rpms 10 fold does not drop conversion equivalently
- gas flowrate does a lot of the heavy lifting with regards to mixing compared to the stirrer
- velocity that disturbs the liquid enough to act as a mixer itself

How much energy can we save?

- Scaled concentration until performance dropped – managed to increase substrate up to 20%.
- This means that we can reduce distillation energy costs by 60%
- Lab scale tests and model indicates that:
 - 140 kWh/kg of product using current procedure
 - 13 kWh/kg of product using developed flow
- That's an 11 fold reduction in energy this step

Next Step: Scaling



Current scaled design utilises similar number of tanks and baffled interior so that micro mixing time is matched at scale

Fortunately managed to optimised conditions without significant pressure
- Allows for CAPex saved

Pilot testing begins in Feb!

Process only takes 48
hours

Yield Increased to 80%

Revenue doubled

11 fold Energy reduction

Scaling up in Feb!

