



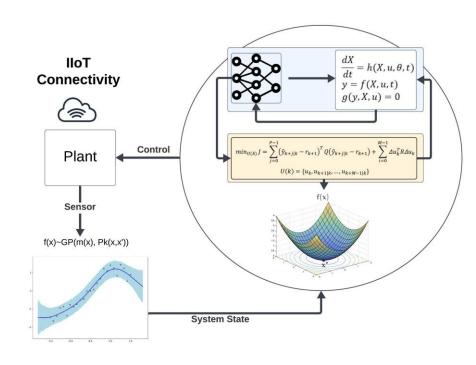
Bioprocessing 4.0: Minimising Cost of mRNA Vaccine Manufacturing

Kesler Isoko a,b, Mahdi Ahmed b, Joseph Middleton b, Joan L. Cordiner b, Zoltan Kis b,c*, Peyman Z. Moghadam a*

a Department of Chemical Engineering, University College London, Torrington Place, London WC1E 7JE, United Kingdom

b School of Chemical, Materials and Biological Engineering, University of Sheffield, Mappin Street, Sheffield S1 3JD, UK

c Department of Chemical Engineering, Imperial College London, South Kensington Campus, London SW7 2AZ, UK





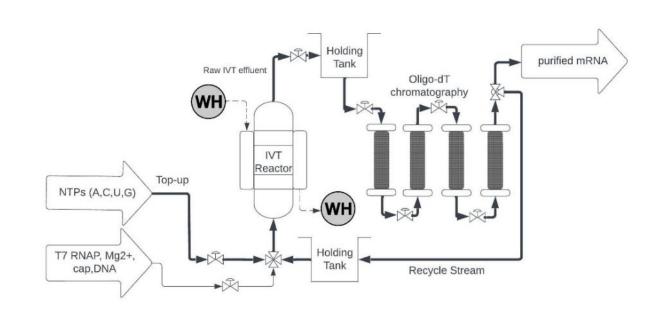
The Goal: Recycling Expensive Raw Materials

Opportunity

 Recycling expensive reagents could significantly reduce the cost of mRNA (2-5x)

Problem

 However, this process is still very manual, and the high dead-times, low observability make it challenging to control





Control Setup in mRNA Recycling

MPC Controller

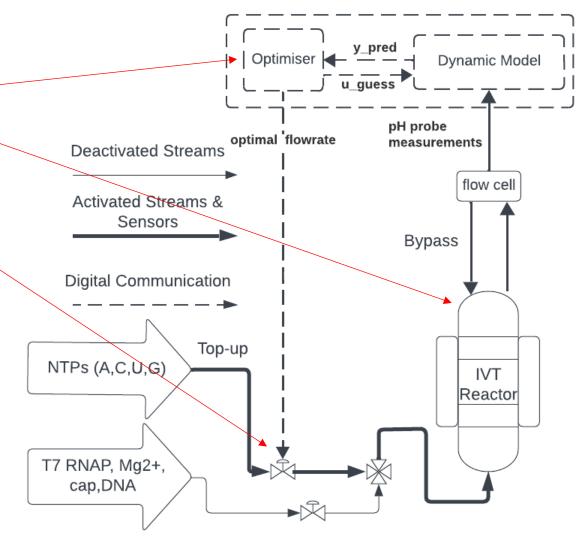
Variable Names	Notation	Example
Prediction Horizon	Р	Number of steps the model predicts
Control Horizon	М	Number of control actions evaluated
Control Outputs	Υ	RNA yield
Reference Trajectory	r	Desired Yield Response
State Variables	Х	Other Components i.e. DNA Template
Control Inputs	U	NTPs Valve Position

Measurements

pH can be used to monitor the reaction

Objective

 Our goal is to feed NTP such that we maximise yield with minimum side-effects such as pyrophosphate ions production





Control Setup: Dynamic Model

Variable Names	Notation	Example
Prediction Horizon	Р	Number of steps the model predicts
Control Horizon	М	Number of control actions evaluated
Control Outputs	Υ	RNA yield
Reference Trajectory	r	Desired Yield Response
State Variables	Х	Other Components i.e. DNA Template
Control Inputs	U	NTPs Valve Position

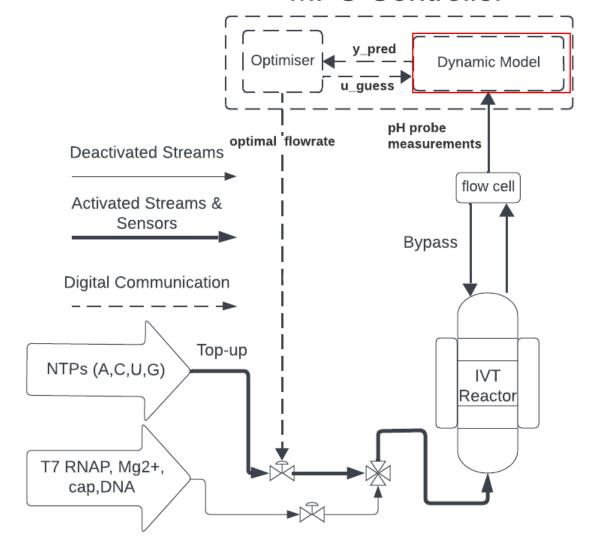
Measurements

pH can be used to monitor the reaction

Objective

 Our goal is to feed NTP such that we maximise yield with minimum side-effects such as pyrophosphate ions production

MPC Controller





Dynamic model development: Data Driven

Purely data-driven (System identification)

- AutoRegressive with eXogenous inputs (ARX)
- Nonlinear AutoRegressive with eXogenous inputs (NARX)
- Neural Networks (RNN, LSTMs, etc...)

Purely Mechanistic (with state estimation)

- Extended Kalman Filters (EKF), Unscented Kalman Filters (UKF), Kalman Filters (KF)
- Process Analytical Technologies (PAT)
- Soft sensors

Hybrid semi-parametric modelling

- Serial
- Parallel

Pros of data-driven

- No first principal knowledge required
- Linear models generates a quadratic optimisation programme (convex) that can be solved reliably online

Cons of data-driven

- ARX Might not capture nonlinear dynamics leading to instability
- Requires enough step response data or access to plant to calibrate dead-time, rise-time and steady states parameters



Control Setup: Dynamic Model

Variable Names	Notation	Example
Prediction Horizon	Р	Number of steps the model predicts
Control Horizon	М	Number of control actions evaluated
Control Outputs	Υ	RNA yield
Reference Trajectory	r	Desired Yield Response
State Variables	Х	Other Components i.e. DNA Template
Control Inputs	U	NTPs Valve Position

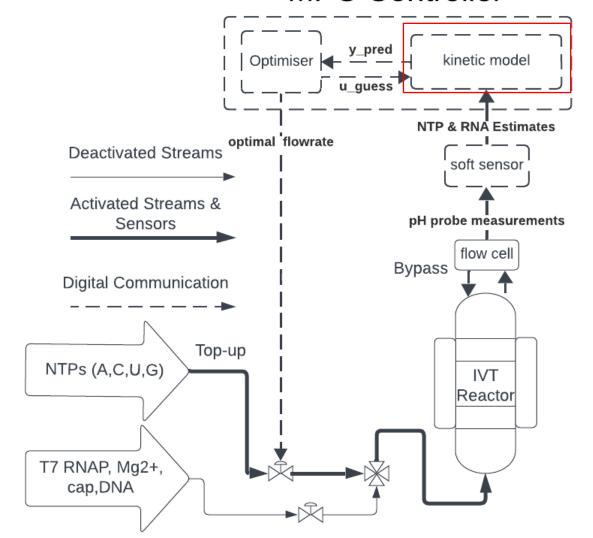
Measurements

pH can be used to monitor the reaction

Objective

 Our goal is to feed NTP such that we maximise yield with minimum side-effects such as pyrophosphate ions production

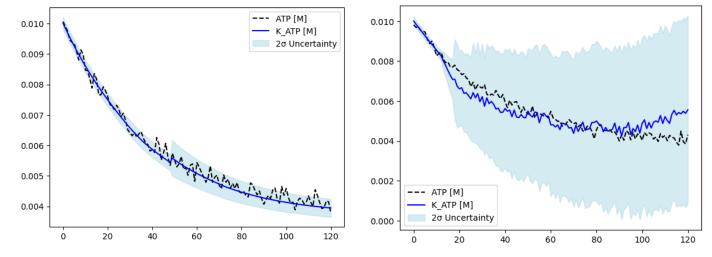
MPC Controller

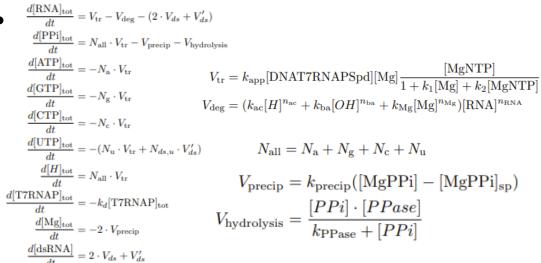




Dynamic model development: Mechanistic

- Purely mechanistic
- Moving Horizon Estimation
- PAT
- Soft sensor for key variables



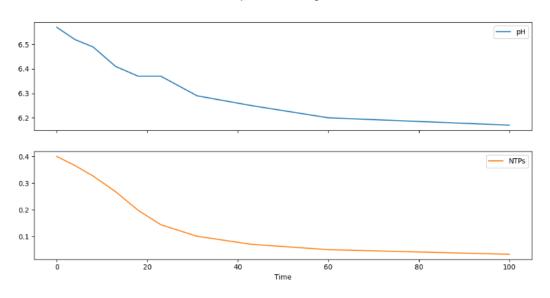


- Linearisation techniques lead to poor performance (EKF)
- UKF is accurate however requires proper calibration and is too slow to be integrated in optimisation loop



Developing a PAT sensor





$$pH = pK_a + \log\left(\frac{[A^-]}{[HA]}\right)$$

Pros

Provides accurate estimates of NTP & RNA

Cons

- Numerical instability of the log in python due to floating point errors
- Sensitive to noisy measurements



Soft sensor development: Physics-informed Gaussian Process Regression

Requirements

- Keep the physics
- Sampling efficient
- Robust to noisy measurements

Gaussian Processes

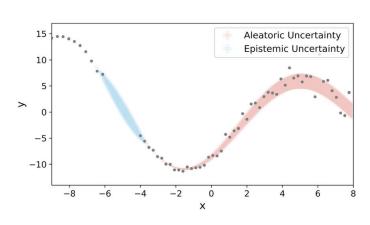
- Follow a Bayesian formulation
- Require little data
- Uncertainty Quantification

$$f(\mathbf{x}) \sim \mathcal{GP}\left(m_f(\mathbf{x}), k_f(\mathbf{x}, \mathbf{x}')\right)$$

$$\kappa(x_i, x_j) = \exp\left(-\frac{\left\|x_i - x_j\right\|^2}{2\sigma^2}\right)$$

$$pH = pK_a + \log\left(\frac{[A^-]}{[HA]}\right)$$

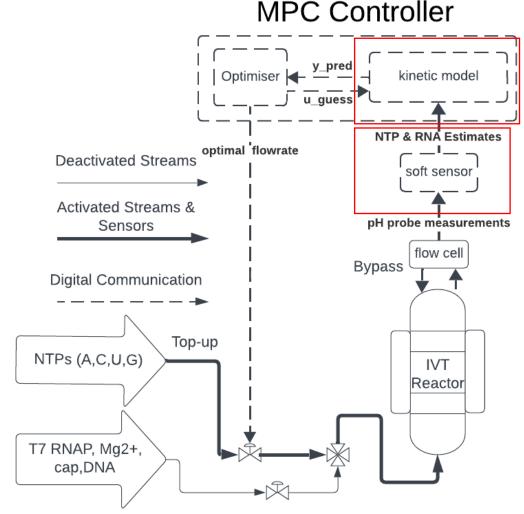
$$k(x_i, x_j) = \exp\left(\frac{\left|\left|\log(1 + |x_i - pK_a|) - \log(1 + |x_j - pK_a|)\right|\right|^2}{2\sigma^2}\right) + \alpha * \delta_{ij}$$





Soft sensor development: Physics-informed Gaussian Process Regression

- Two models deployment (complicated setup)
- Error can carry over leading to unnecessary instability
- Kinetic model performance was unsatisfactory





Control Setup: Hybrid Model

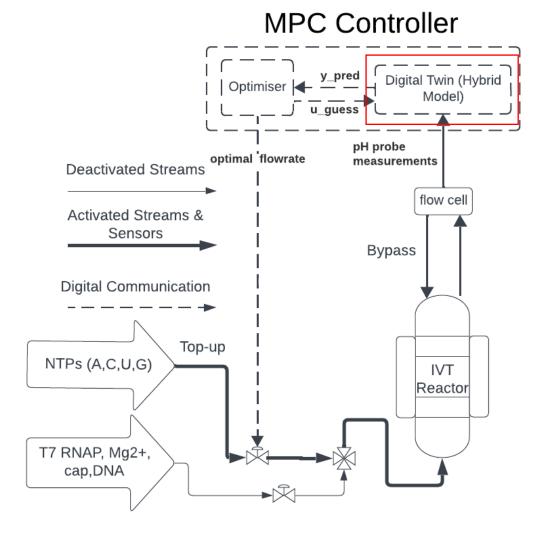
Variable Names	Notation	Example
Prediction Horizon	Р	Number of steps the model predicts
Control Horizon	М	Number of control actions evaluated
Control Outputs	Υ	RNA yield
Reference Trajectory	r	Desired Yield Response
State Variables	Χ	Other Components i.e. DNA Template
Control Inputs	U	NTPs Valve Position

Measurements

pH can be used to monitor the reaction

Objective

 Our goal is to feed NTP such that we maximise yield with minimum side-effects such as pyrophosphate ions production





Dynamic model development: Hybrid Model

Hybrid semi-parametric model

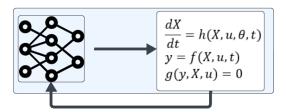
- Serial structure (ensemble)
- Parallel structure (discrepancy, hierarchical)

Methodology

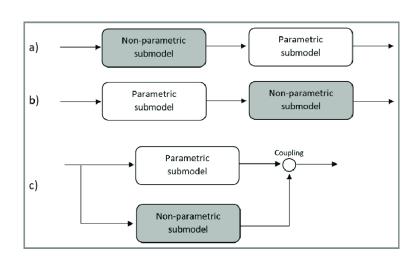
$$\begin{split} \frac{d[\text{RNA}]_{\text{tot}}}{dt} &= V_{\text{tr}} - V_{\text{deg}} - (2 \cdot V_{ds} + V_{ds}') \\ \frac{d[\text{PPi}]_{\text{tot}}}{dt} &= N_{\text{all}} \cdot V_{\text{tr}} - V_{\text{precip}} - V_{\text{hydrolysis}} \\ \frac{d[\text{ATP}]_{\text{tot}}}{dt} &= -N_{\text{a}} \cdot V_{\text{tr}} \\ \frac{d[\text{GTP}]_{\text{tot}}}{dt} &= -N_{\text{g}} \cdot V_{\text{tr}} \\ \frac{d[\text{CTP}]_{\text{tot}}}{dt} &= -N_{\text{c}} \cdot V_{\text{tr}} \\ \frac{d[\text{UTP}]_{\text{tot}}}{dt} &= -(N_{\text{u}} \cdot V_{\text{tr}} + N_{ds,u} \cdot V_{ds}') \\ \frac{d[\text{H}]_{\text{tot}}}{dt} &= N_{\text{all}} \cdot V_{\text{tr}} \\ \frac{d[\text{T7RNAP}]_{\text{tot}}}{dt} &= -k_{d}[\text{T7RNAP}]_{\text{tot}} \\ \frac{d[\text{Mg}]_{\text{tot}}}{dt} &= -2 \cdot V_{\text{precip}} \\ \frac{d[\text{dsRNA}]}{dt} &= 2 \cdot V_{ds} + V_{ds}' \end{split}$$

$$f(\mathbf{x}) \sim \mathcal{GP}\left(m_f(\mathbf{x}), k_f(\mathbf{x}, \mathbf{x}')\right)$$

$$\kappa(x_i, x_j) = \exp\left(-\frac{\|x_i - x_j\|^2}{2\sigma^2}\right)$$



$$WMSE = \frac{1}{T} \sum_{t=1}^{T} \frac{(c_t^* - c_t)^2}{\sigma_t^2}$$
 Levenberg-Marquardt (LMM algorithm



Evaluated ALL the relevant ML techniques

- Support Vector Regression
- Bayesian Regression
- Gaussian Processes
- Xgboost, Random Forest, LightGBM
- Linear Regression, ElasticNet
- Partial Least Squares



Control Setup: Optimiser

Variable Names	Notation	Example
Prediction Horizon	Р	Number of steps the model predicts
Control Horizon	М	Number of control actions evaluated
Control Outputs	Υ	RNA yield
Reference Trajectory	r	Desired Yield Response
State Variables	Х	Other Components i.e. DNA Template
Control Inputs	U	NTPs Valve Position

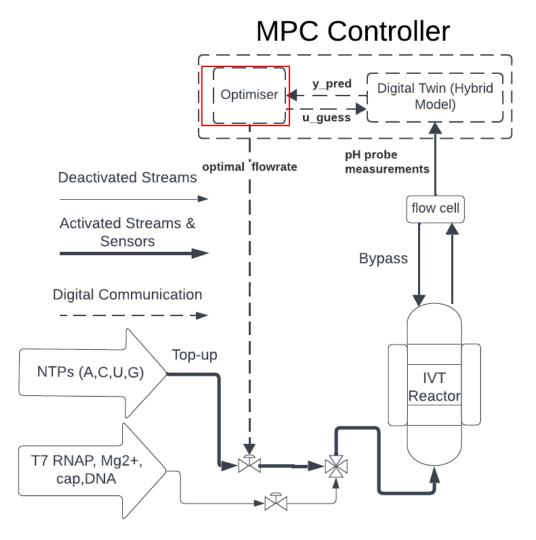
Measurements

pH can be used to monitor the reaction

Objective

 Our goal is to feed NTP such that we maximise yield with minimum side-effects such as pyrophosphate ions production

$$min_{U(k)}J = \sum_{i=0}^{M-1} \Delta u_k^T W_1 \Delta u_k + \sum_{j=0}^{P-1} (\hat{y}_{k+j|k} - r_{k+1})^T W_2 (\hat{y}_{k+j|k} - r_{k+1}) + \sum_{i=0}^{M-1} u_k^T W_3 u_k$$





MPC Controller Design: Tuning Parameters

Metrics

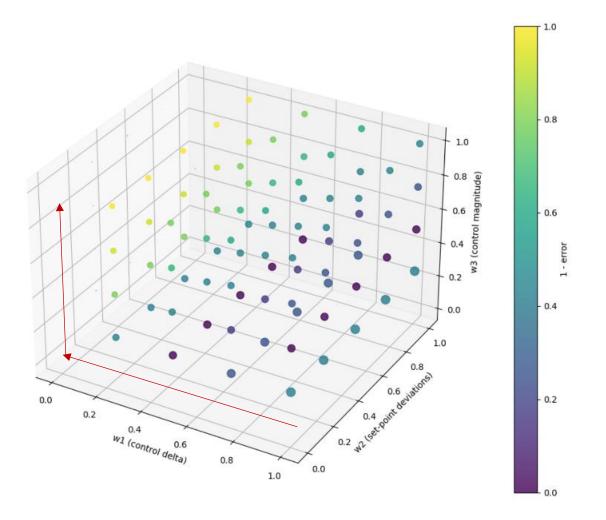
- Colour Steady state performance
- Size Control Effort

Factors

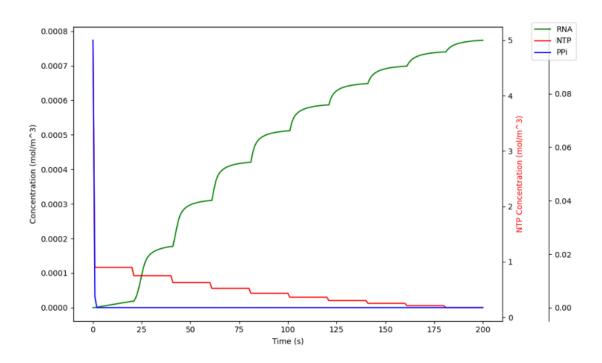
- *W*₁– control delta Significant impact
- W_2 reference trajectory No impact on performance
- W_3 control magnitude Significant impact

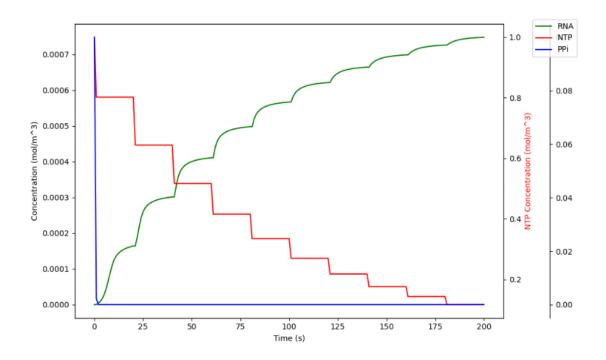
Note

 Reference trajectory range was not physically meaningful therefore, we will need to adopt economic MPC



MPC Controller Design: Control Effort





Methodology

- W₁ control delta
- *W*₂- reference trajectory
- W₃ control magnitude

$$min_{U(k)}J = \sum_{i=0}^{M-1} \Delta u_k^T W_1 \Delta u_k + \sum_{j=0}^{P-1} (\hat{y}_{k+j|k} - r_{k+1})^T W_2 (\hat{y}_{k+j|k} - r_{k+1}) + \sum_{i=0}^{M-1} u_k^T W_3 u_k$$



Control Setup: Connectivity

Variable Names	Notation	Example
Prediction Horizon	Р	Number of steps the model predicts
Control Horizon	М	Number of control actions evaluated
Control Outputs	Υ	RNA yield
Reference Trajectory	r	Desired Yield Response
State Variables	Х	Other Components i.e. DNA Template
Control Inputs	U	NTPs Valve Position

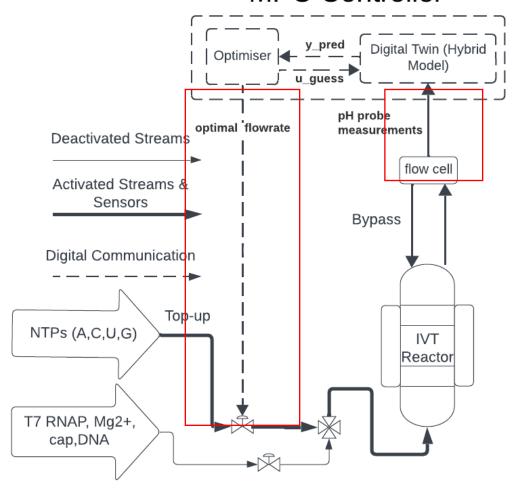
Measurements

pH can be used to monitor the reaction

Objective

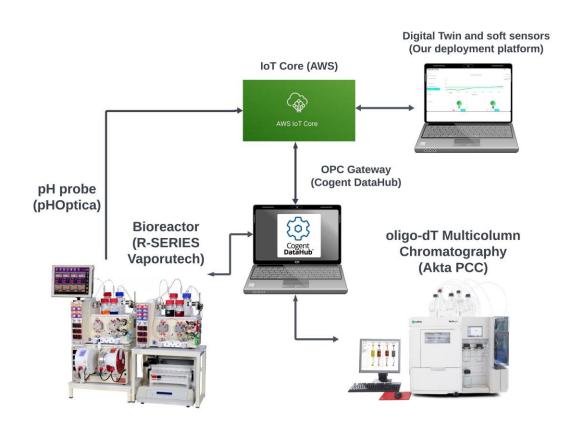
 Our goal is to feed NTP such that we maximise yield with minimum side-effects such as pyrophosphate ions production

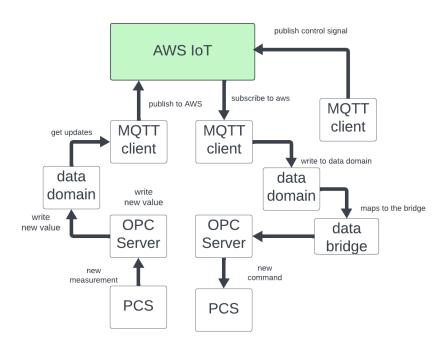
MPC Controller





Industrial IoT Platform: Model Deployment and Connectivity





Methodology

- OPC for interoperability
- MQTT for lightweight robust communication



IIoT Platform Test Feedback

Test Type I errors (False Positives)

Step 1: Increase Mg2+ flowrate to 1.25 L/min. (SAFE)

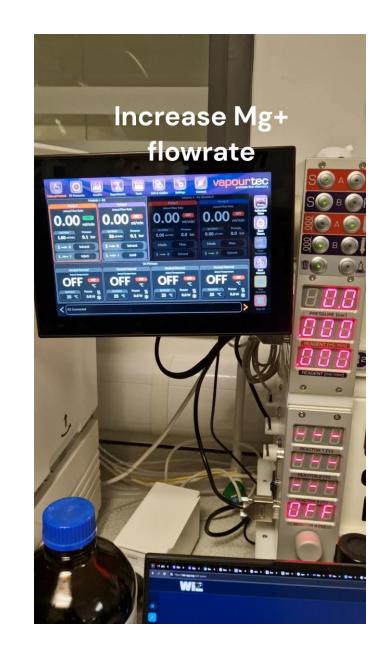
Step 2: Check new RNA yield prediction (≈7 g/L) within acceptance ranges so reaction continues.

Test Type II errors (False Negative)

Step 3: Increase Mg2+ flowrate to 2.00 L/min. (PRECIPITATION)

Step 4: Check new RNA yield prediction (≈5 g/L) outside acceptance ranges.

Step 5: The model shuts down the reaction (Set minimum flowrate to 50 μ L/min to prevent bad batch)





IloT Platform Soft Sensor Deployment





Results Hybrid model

accuracy: 85% in forecasting RNA yield

Soft sensor

accuracy: 90% in estimating current NTPs & RNA concentrations

IIoT Platform Features:

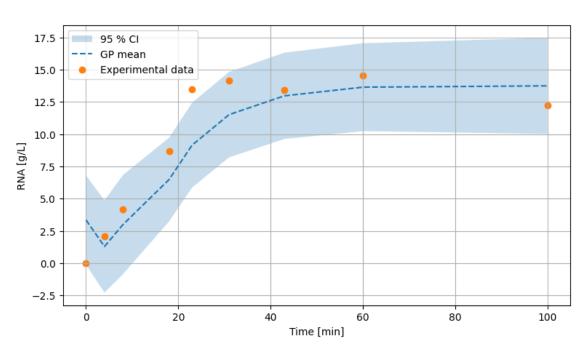
- model deployment
- two-way data connectivity
- real-time visualisation

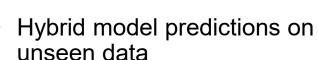
MPC Controller

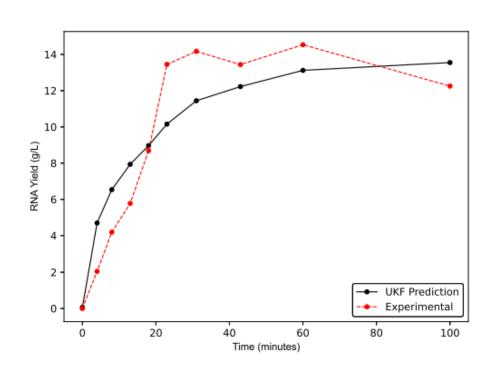
Reduce Costs by 31% vs recycling w PID (85% vs Traditional)



Results Hybrid Model vs Mechanistic Model





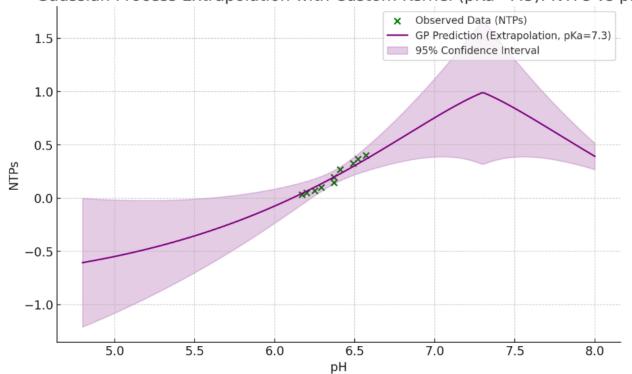


 Mechanistic model predictions on unseen data

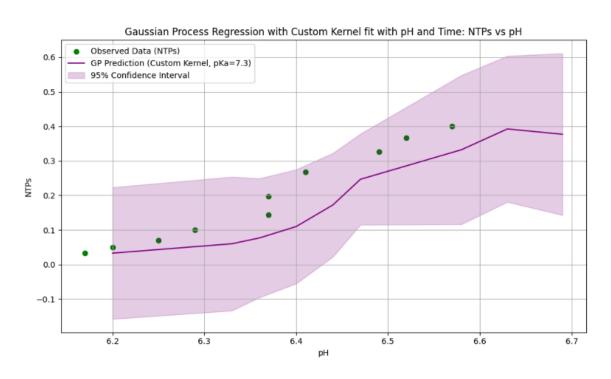


Results: soft sensor





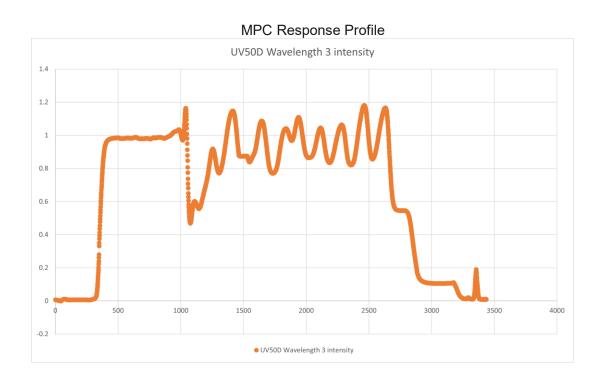
Ceiling constrained successfully!

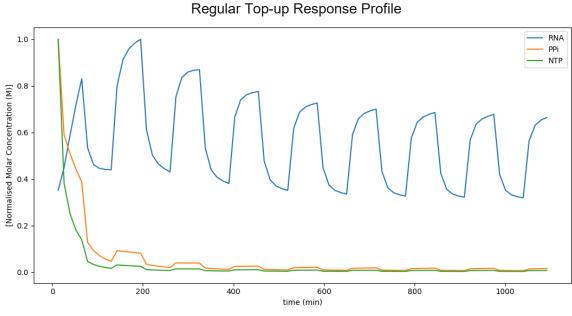


Non-linear relationship between pH and NTPs



Results: Plant Simulator

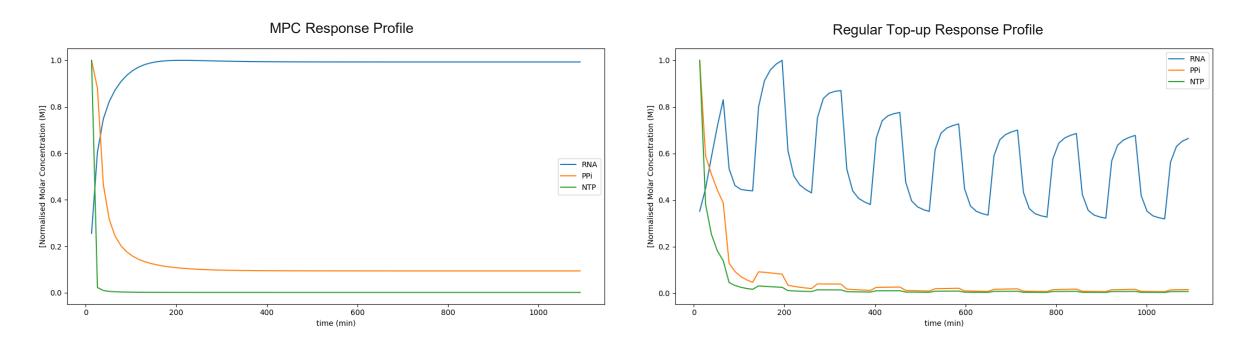




- Plant simulation captures oscillatory dynamics in experimental data
- Quantitative evaluation of the plant required



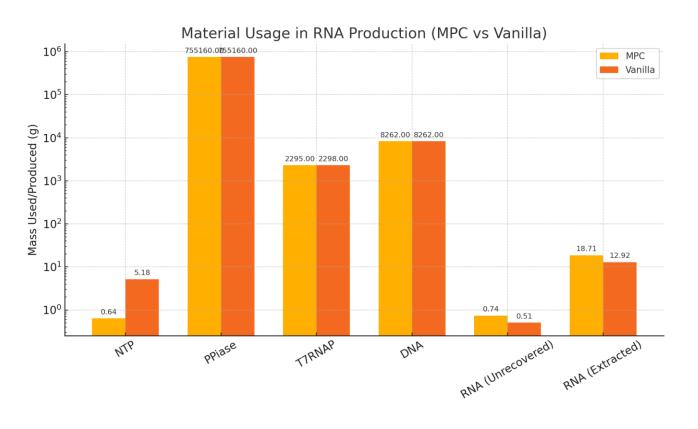
Results: Multi-objective optimisation



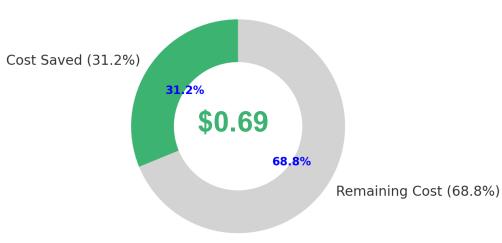
- Model Predictive Controller minimises impurity (PPi)
- MPC controller also maximises yield and maintains optimal operations
- · MPC controller achieves better stability and faster steady-state



Results: Multi-objective optimisation



MPC Cost Savings per g RNA (Relative to Vanilla)



- MPC costs \$0.69 on the dollar compared to standard recycling
- Compared to traditional (no recycling) is
 < 15% of the cost
- MPC makes use of manipulated variables (NTPs) much more effectively
- This leads to higher yields of RNA using less reagent



Summary & Future Work

Summary

- Developed dynamic hybrid model and soft sensors for real-time predictions
- Achieved multi-objective optimisation
- Tested the control strategy in simulation demonstrating cost savings
- Deployed dynamic model in predictive mode via a custom IIoT Platform

Future Work

- Implement Economic MPC with GP-ARX model in the close-loop
- Use Bayesian Optimisation to tune controller parameters
- Deploy full-controller



Acknowledgments Thanks for listening Any Questions?

Funding: Wellcome Leap R3 Programme, CEPI, H. Walter Stern Scholarship

Collaborators: Kesler Isoko, Mahdi Ahmed, Joseph Middleton, Joan L. Cordiner, Zoltan Kis, Peyman Z. Moghadam